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Your reference

JTS\P13232GB

28DEC03 E861926-1 D00239 P01/7700 0.00-0329920.3 NDNE

Patent application number (The Patent Office will fill in this part)

2 4 DEC 2003

0329920.3

Full name, address and postcode of the or of each applicant (underline all surnames)

Axiom Process Limited Central Square South Orchard Street Newcastle Upon-Tyne NE1 3XX

Patents ADP number (if you know it)

If the applicant is a corporate body, give the country/state of its incorporation

856 1565001

Title of the invention

Screening Apparatus

Name of your agent (if you have one)

"Address for service" in the United Kingdom to which all correspondence should be sent (including the postcode)

Cruikshank & Fairweather

19 Royal Exchange Square Glasgow, G1 3AE Scotland, UK

547002

Patents ADP number (if you know it)

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Country

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Number of earlier application

Date of filing (day / month / year)

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23 December 2003

12. Name and daytime telephone number of person to contact in the United Kingdom

Mr Jan T Szczuka - 0131 225 4500

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SCREENING APPARATUS

The present invention relates to vibratory screening

5 apparatus suitable for use with drilling fluids and the like.

Vibratory screening apparatus is widely used in the oil drilling industry for removing drill cuttings from drilling fluids, and over the years various improvements have been made to the screens used therein, methods for mounting the screens etc to improve ease of use, reduce maintenance etc. A particular problem in offshore platform oil drilling is, however, that platform real estate is very restricted and extremely expensive. There is accordingly a need to improve the efficiency of vibratory screening apparatus in relation to the physical size thereof.

The present invention provides a vibratory screening apparatus for use in removing solids from a liquid and solids mixture feed, said apparatus comprising a static outer housing, at least one floating basket mounted so as to be vibratable, in use of the apparatus, by a vibrator device formed and arranged for vibrating said basket, said basket mounting a stack of screen assemblies separated by flow directing trays, said apparatus being provided with a flow distributor formed and arranged for dividing said feed into at least a first feed stream and a second feed stream and directing said feed streams onto respective ones of first and second screen assemblies, and receiving from respective flow

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directing trays, respective filtrates from said respective screen assemblies.

With an apparatus of the present invention, the size of apparatus required to process a given volume of feed is substantially reduced compared with conventional apparatus, since a substantially increased effective screen surface area can be accommodated with relatively little or no increase in the size of the apparatus by means of stacking a plurality of screen assemblies within a single basket and using a flow distributor to route multiple flows in parallel through different screens in the stack.

Advantageously the distributor is formed and arranged so as to be switchable between a plurality of different flow directing configurations. Conveniently said plurality of flow directing configurations includes an intensive screening configuration in which the whole of the feed is directed onto said first screen assembly and the whole of the filtrate from said first screen assembly is directed onto said second screen assembly. Alternatively or additionally there is provided a restricted feed capacity configuration in which the whole of the feed is directed onto only one of said first and second screen assemblies, and the filtrate therefrom exhausted directly from the apparatus without passing through the other one said first and second screen assemblies. Such a configuration is useful for basic fluid processing where high efficiency or high volume processing are not required

and a reduced number of screens in operation reduces operating cost for screens consumed.

Advantageously the mesh sizes of the various screens are selected to suit the particular distributor configuration being employed and/or the loading of the mixture (% solids content), the particle size of the solids, and/or the particle size distribution of the solids. Thus for example in a configuration where the feed is divided into one portion passing through the first screen and not the second, and another portion passing through the second screen and not the first, the first and second screens would normally have the same mesh size. On the other hand in a configuration where the whole of the feed is passed successively through both the first and second screens, then the second screen would normally have a finer mesh size than the first screen.

In general the distributor will comprise a plurality of passages provided with valves, typically flap valves, sleeve valves or plug valves, or closure plates etc, for selective opening or closing of different passages. The distributor may be mounted in either the static housing or on the floating basket. It is also possible, in principle, for part of the distributor to be mounted in the static housing and part on the floating basket. Where a greater or lesser part of the distributor is mounted in the static housing, then the distributor is generally provided with flexible conduit

portions defining at least part of the passages, for coupling the passages from the static housing to the floating basket.

The passages of the distributor may be defined in various

different ways. Conveniently they are defined by walls
extending downwardly inside a downwardly extending chamber so
as to provide a lateral subdivision of the chamber into
individual passages providing predetermined proportions of
the distributor flow capacity. Thus, for example, the

distributor may be formed and arranged with one or more first
flow passages for transmitting said first feed stream, and
one or more second flow passages for transmitting said second
feed stream.

It is generally preferred that vibratory screen apparatus 15 should have a plurality of screen assembly stages with decreasing mesh size. It will accordingly be appreciated that in addition to having first and second screen assemblies, with similar mesh size, formed and arranged for intercepting said first and second feed streams respectively, 20 the vibratory basket may also have one or more further screen assemblies with different mesh size upstream and/or downstream of said first and second screen assemblies. Conveniently there is provided upstream of first and second screen assemblies, an initial, coarser mesh size, screen assembly and the vibratory screening apparatus is formed and arranged so that substantially the whole of the liquid and solids mixture feed is directed through said initial screen assembly, before being divided into said at least first and

second feed streams. In such cases there would generally be used an initial screen assembly with a mesh size of around 10 to 80 (wires per inch), for example, about 20, and the first and second screen assemblies would have a mesh size of around 40 to 325, conveniently 100 to 250 for example about 200. In yet another possible distributor configuration which could also be provided, the feed is passed only through the initial coarse screen.

10 Various screen assemblies and screen mounting systems may be used in the apparatus and baskets of the present invention, including, for example, those described in our earlier patent publication WO 03/013690.

In a further aspect the present invention provides a basket suitable for use in a vibratory screening apparatus, said basket mounting a stack of screen assemblies separated by flow directing trays, and being provided with a flow distributor formed and arranged for dividing said feed into at least a first feed stream and a second feed stream and directing said feed streams onto respective ones of first and second screen assemblies, and receiving from respective flow directing trays, respective filtrates from said respective screen assemblies.

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Further preferred features and advantages of the invention will appear from the following detailed description given by way of example of preferred embodiments illustrated with reference to the accompanying drawings in which:

Fig. 1 is a schematic sectional elevation of a vibratory screening apparatus of the present invention;

Figs. 2A to 4B are schematic vertical sections illustrating different flow paths through the stacked screens with

5 different configurations of the flow distributor set up for parallel and series operation;

Figs. 5A-C are schematic perspective end views of the basket of the apparatus also illustrating the flow paths in various different configurations of the flow distributor;

10 Fig. 6 is a side elevation of a modified apparatus with a static flow distributor connected to a floating vibratory apparatus;

Fig. 7 is a partly cut-away schematic perspective view of a further embodiment showing one module of a twin-module

15 apparatus set up for parallel operation;

Figs. 8A and 8B are vertical sections of the apparatus of Fig. 7 at A and B; and

Figs. 9-10 are corresponding views of the apparatus of Figs. 7-8, set up for series operation.

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Fig. 1 shows schematically one embodiment of a vibratory screen apparatus 1 of the invention with an outer housing 2 in which is mounted on springs 3 a basket 4. The basket is generally box shaped with pairs of circumferentially

extending inwardly projecting flanges 5 height on the basket side walls 6, for supporting respective ones of a stack 7 of screen assemblies 8 separated by flow directing trays 9. A vibrator unit 10 is secured to the top 11 of the basket. The interior 12 of the basket 4 is divided into a series of

levels 13 between neighbouring screen assemblies 8 and flow directing trays 9.

- Figs. 2 A/B to 4 A/B show schematically a distributor 15

 5 provided at one end 16 of the floating basket 4. The distributor 15 is formed and arranged into inside and outside passages 17, 18 shown in Figs. 2A to 4A, and 2B to 4B, respectively, for connecting with the various levels 13 of the interior 12 of the basket 4 via openings 19 controlled by flap valves 20. In some cases the flap valves 20 are additionally used to control openings 21 along the length of the passages 17, 18 in certain positions of said flap valves 20, as further described hereinbelow.
- 15 Figs 2A/B, 3A/B and 4A/B show different configurations of the distributor 15 for providing different feed flow arrangements through the screen assemblies 8, which are indicated as A, B and C, respectively, in Figs 2 to 5.
- In more detail Fig 2A shows the inside passage 17 and interior 12 of the basket 14, with an upper flap valve 20' raised to open an upper connecting opening 19' connecting the passage 17 and first level 13' above the upper flow deflector tray 9'. An intermediate flap valve 20'' is raised to close an intermediate connecting opening 19'' connecting the passage 17 and second level 13' between the upper and lower flow deflector trays 9', 9'' whilst simultaneously opening an intermediate level opening 21' in passage 17. A lower flap valve 20''' is lowered to open a lower connecting opening

19''' connecting the passage 17 and a fourth level 134 below the lower flow deflector tray 9''. In this configuration it may be seen that a feed 22 of liquid and solids is passed through a coarse mesh, (typically mesh size 20) upper screen 8' and the filtrate 23 passed along the upper flow deflector tray 9' into passage 17 and thence, bypassing a first, midlevel, screen 8'', onto a second, low-level, screen 8''. In this configuration the whole of the feed 22 is passed through the coarse screen 8' and only one of the first and second screens 8'',8'''.

Figs. 3B shows the distributor 15 configured so that the upper flap valve 20' is raised to open the upper connecting opening 19', the intermediate flap valve 20'' is lowered to open the intermediate connecting opening 19'' whilst simultaneously closing the intermediate level passage opening 21', and the lower flap 20''' is lowered to open the lower connecting opening 19''! whilst closing a bottom passage opening 21'' as before. In this configuration the whole of the feed 22 is passed through the coarse screen 8' and then successively through each of the first and second screens 8'', 8''' thereby providing a more progressively finer screening of the feed (by using a finer mesh size in the second screen than in the first screen).

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Fig. 4A shows the distributor in the inside passage 17 configured so that the upper flap valve 20' is raised as before. The intermediate flap valve 20'' is lowered so as to open the intermediate connecting opening 19'' whilst

simultaneously closing the intermediate level passage opening 21' and the lower flap 20''' is raised to close the lower connecting opening 19''' whilst opening the bottom passage opening 21'''. In this configuration of the inside passage 17 in the distributor 15, that part 23' of the filtrate 23 from the coarse screen 8' passing into the inside passage 17, is directed onto the first screen 8'' and then out of the bottom opening 21'' of the inside passage 17, by-passing the second screen 8'''. The outside passage 18 is configured as in Fig. 2A so that the remaining part 23'' of the filtrate 23 from the coarse screen 8' passing into the outside passage 18, is directed onto the second screen 8''' by-passing the first screen 8''. It will be appreciated that in this configuration of the distributor 15, the screen area 15 available for screening of the feed 22 is effectively double that used in Fig. 2A/B and that available in a conventional vibratory screening apparatus basket of similar footprint.

- Figs. 5A C are schematic perspective views of the end 16 of 20 the basket 4 to which the distributor 15 is coupled but with the distributor 15 substantially removed for clarity, showing the flows in and out of the various openings 19 connecting the distributor 15 to the interior 12 of the basket 4.
- 25 Fig. 6 shows schematically another embodiment in which there is used a distributor 24 mounted on the static housing 2 and with its connecting openings 19 coupled to the corresponding levels 25 inside the floating basket 4 by flexible conduits 26.

Fig. 7 shows a further embodiment of a screening apparatus 27 of the invention which has identical twin modules 28, 29 (only one shown in detail). Each module has a first, coarse mesh, upper, scalping, deck 30 with a first, coarse mesh, screen 31 above a flow back tray 32. Fluid 33 to be screened is retained on the screen 31 by an end wall 34.

Below the first deck tray 32 is disposed a second deck 35

10 comprising a second screen 36 above a respective flowback tray 37. A certain amount of fluid 38 is retained on the second screen 36 by a weir 39 provided at the lower end 40 thereof. When the flow rate of the feed of fluid 33 to be screened, exceeds the capacity of the second screen, part 41 of the fluid 38 overflows the weir 39 either directly into one or other of two vertically extending conduits 42 at opposite sides of the module 28, or onto one or other of two sloping deflector plates 43 which divert it into a respective one of the conduit 42, as shown by the single headed fluid 10 flow arrows in Figs. 7-8.

At the bottom 44 of the vertical conduits 42 are provided rearwardly facing openings 45 through which the diverted fluid 41 is directed onto the screen 46 of a third deck 47 disposed below the second deck 35. Thus this part 41 of the fluid flow 33 passes through the first deck screen 31 and the third deck screen 46, by-passing the second deck screen 36 (see also Figs. 8A and 8B, in which Fig. 8A is a section through a central vertical plane at A, which extends through

a central portion 48 of the module 28, with the deflector plates 43; and Fig. 8B is a vertical section through one of the vertically extending side conduits 42).

- That part 38 of the fluid 33 retained on the second screen 36 is passed through the second deck screen 36 (the solid particulate material 49 retained thereon being ``walked up'' the screen 36 in the usual way - see Fig. 8B), as indicated by the double headed arrows 50. This part 50 of the fluid 10 flow 33, is then passed through a second deck end wall opening 51 and down a central vertically extending conduit 52 underneath the deflector plates 43. A closure panel 53 seals a third deck end wall opening 54, below the second deck end wall opening 51, thereby preventing this part 50 of the fluid flow 33 from entering the third deck 47. A bottom opening 55 in the central vertical conduit 52 allows this fluid flow 50 to pass into the sump 56 of the apparatus 28 where it rejoins the other part 38 of the fluid flow 33, the respective parts 41 and 38, 50 of the fluid flow 33, being passed through the first deck screen 31 and then, in parallel, through a respective one of the second and third deck screens 36, 46.
- The module 28 as described above, may be readily reconfigured for serial operation whereby the whole of the fluid is passes through each one of the first, second and third deck screens, 31, 36, 46, as shown in Figs. 9-10. In more detail the weir 39 is replaced by a high wall 57 which ensures that the whole of the fluid flow 33 is passed through the second deck screen 36. As before, the fluid flow 58 then passes out through the

second deck end wall opening 51 into the central vertical conduit 52. In this configuration, the bottom opening 55 is sealed by a closure plate 59 whilst the closure panel 53 of the third deck end wall opening 54 is opened so that the fluid flow 58 is routed from the central vertical conduit 52 into the third deck 47 and passed through the screen 46 thereof into the sump 56.

Each of the first and second modules 28, 29, would normally be configured in the same way, but if desired they could be 10 configured differently i.e. one for parallel (2 screen) operation and one for series (3 screen) operation. Also single screen operation is possible when required, by removing one or two screens from the or each module depending on the configuration of the modules and the fluid feed arrangement. In addition the fluid feed to the apparatus can be arranged to be directed to either or both of With the significantly increased fluid the modules. processing capacity of the apparatus (in parallel mode) it will be appreciated that occasions will arise when the fluid 20 feed is insufficient to maintain a high fluid level and short beach length on the screens, which can result in drying of the particulate solids on the beach portion of the screen and damage to the screens therefrom. In such circumstances damage to the screens can be minimized by restricting the 25 fluid feed to only one of the twin modules.

A particular advantage of this type of embodiment is that, in its parallel configuration, a more even and controlled

distribution of the fluid flow across the width of the module is obtained, thereby providing a more efficient screening.

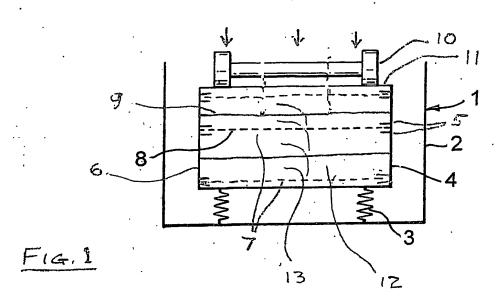
Another significant advantage is a significantly increased fluid screening capacity - which can approach almost 100% greater than with conventional screening apparatus of the same footprint.

It will also be appreciated that various parameters of the modules may be made further configurable. Thus, for example, the weir height could be configurable for a series of different heights. Also the relative proportions of the central and side, vertical conduits could be selected to accommodate particular desired flow capacity proportions for the different fluid flow parts in parallel mode operation.

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It will further be appreciated that various modifications may be made to the above embodiments without departing from the scope of the present invention. Thus, for example, in place of a flow distributor system based on the use of closure

20 plates and/or flap valves, there could be used one based on proportional valves and the like.



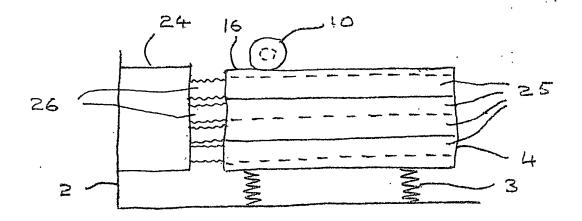
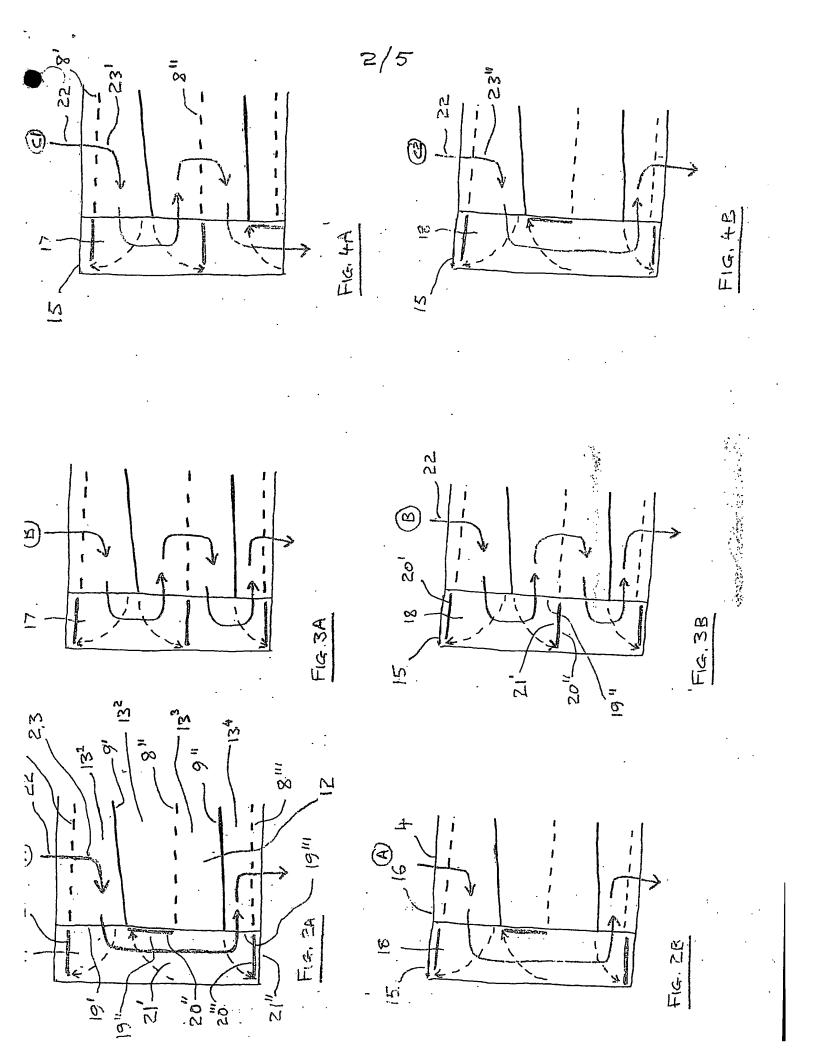


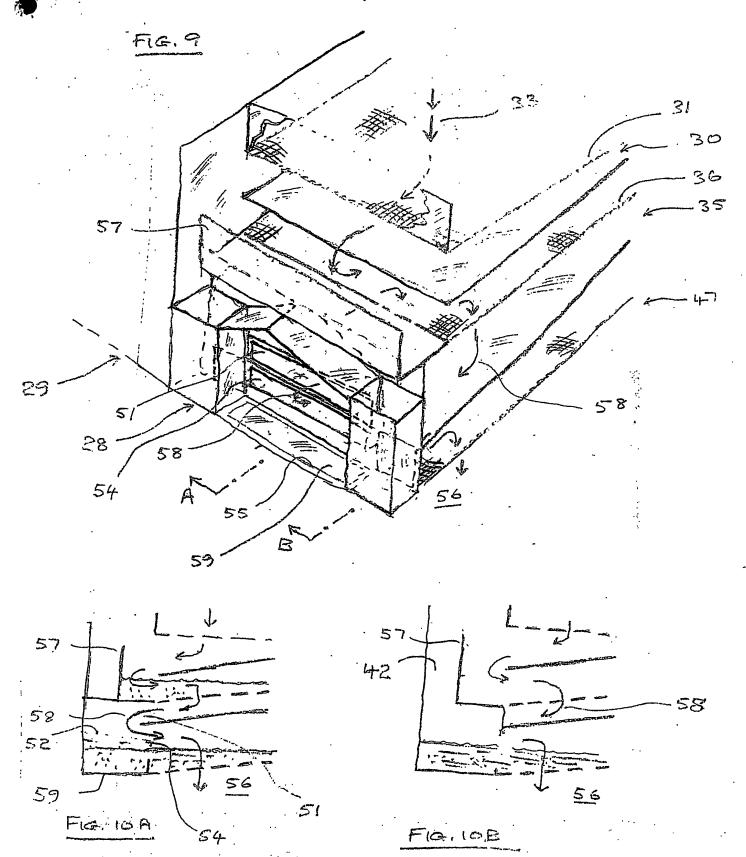
FIG. 6



9 43

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